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## THERMODYNAMIC PROPERTIES OF 1-PENTANOL AT ATMOSPHERIC PRESSURE

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Data is generalized on the density, sonic velocity, and isobaric specific heat of liquid 1-pentanol and calculations are made of the isochoric specific heat, coefficients of adiabatic and isothermal compression, and enthalpy in the temperature range 194.95-411.13°K.

This study is a continuation of our work [1, 2] on analyzing, systematizing, and succintly representing experimental information on the thermodynamic properties of monohydric aliphatic alcohols.

The following equation was chosen as the approximating function to describe the temperature dependence of density, sonic velocity, and isobaric specific heat from the normal melting point up to the boiling point:

$$y = \sum_{i=0}^{n} a_i \tau^i, \tag{1}$$

where  $\tau = T/1000$ , while y respectively denotes  $\rho^{-1}$ , W, and  $C_p$ .

The coefficients  $a_i$  of Eq. (1) for  $\rho^{-1}$ , W, and  $C_p$  were determined by the least-squares method on the "Minsk-32" computer.

<u>Density.</u> Numerical data on the density of liquid 1-pentanol has been systematized in several handbooks [3-5]. The available empirical data on density at atmospheric pressure and on the saturation curve for the period before 1970 was generalized in the survey [4] in the form of a Francis equation. This equation describes initial values within the estimated error and is valid in the temperature range  $253-393^{\circ}K$ . Of the recommended values of  $\rho$  [4], the most accurate are those for 293.15 and 298.15°K, the averaging error for which was evaluated as  $\pm 0.0002$  and  $\pm 0.0003$  g/cm³. Comparison of the results of the generalization in [4] with later (1976) measured densities on the saturation curve [5] obtained at 293-490°K with an error less than 0.02% shows that they do not agree well with each other. Whereas the deviation at T = 293.15°K is 0.04%, it increases with temperature and reaches 0.5% at T = 393.15°K. Here, the values of density are too high in every case.

In the low-temperature range there is a limited amount of experimental data. The study [6] measured density on the saturation curve in the temperature range from 213 to 453°K with an error on the order of 0.1%. Comparison of the data in [5] and [6] shows that at 293-393°K the values agree to within 0.10-0.15% except for one point at T = 393.15°K, for which the de-

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TABLE 1. Coefficients of Eq. (1)

Coefficient a <sub>i</sub>	Property			
	ρ-1	W	$C_P$	
$a_0$	0,919493696	3279,97421	31,8377532	
$a_1$	0,955010991	-14093,9248	689,310441	
$a_2$	2,15274778	42126,3745	6465,89767	
$a_3$	<del>-11,8569303</del>	-71340,7378	-31713,6573	
$a_4$	19,2229056	43524,8023	85573,0936	
$a_5$	<b>—</b> ,	_	-119647,448	
$a_6$	_		67590,6073	
Temperature				
range, K	194,95—411,13	200-404	198,15-411,1	

viation is 0.51%. The study [7] reported densities on the saturation curve at temperatures from 232.95 to 423.1°K. These values were obtained by the authors by graphical-analytical extrapolation of their data on density, measured to within 0.1% for 99.90% by wt. alcohol at higher pressures, to the saturation curve. Finally, the investigation [8] measured density at the melting point ( $\delta \rho \simeq 0.1\%$ ).

As concerns the data [9-12], preliminary comparison of these results with the most reliable values [5] at T > 293°K showed that the deviations for them were within the range 0.1-0.5%. The range was significantly higher for some empirical points [12], a fact which seriously increases the total error of the values being compared. For example, the results in [9] are too high by an average of 0.1%, while the data in [10] and [11] is overstated by 0.5 and 0.2%, respectively.

The set of initial data that was analyzed included the results from [3-8, 13, 14], with priority here having been given to the results in [5]. The density values on the saturation curve [4-7] were corrected for atmospheric pressure by the method proposed in [2]. The size of the correction did not exceed 0.01%.

The values found for the coefficients  $\alpha_i$  for Eq. (1) are shown in Table 1. Figure la compares density values calculated from Eq. (1) with the initial empirical values. It can be seen from the figure that the deviations lie within the experimental error in these studies. Results of comparison with values obtained in [15] at T = 292-379°K to within 0.1% show their good agreement within the range  $\pm 0.01-0.03\%$ . However, if we consider that the measurements in [15] were made for 99.5% (by wt.) alcohol, then the agreement is not as good if we recalculate for a 100% concentration. This is indirectly confirmed by the results obtained in [16], in which special measurements at T = 293.15°K for methanol and ethanol showed that a slight water impurity (0.026% by wt.) in them increases density by about 0.01%. Similar results were obtained in [17] for propanol-1.

The possible error of the recommended density values in Table 2, calculated from (1) in the temperature range from the melting point (T = 194.95°K [4]) to the boiling point (T = 411.13°K [5]) at atmospheric pressure (101325 Pa), can be evaluated as  $\pm 0.02\%$  at T  $\gtrsim$  293°K,  $\pm 0.05\%$  at 253 < T < 293°K, and 0.10-0.15% at T  $\lesssim$  253°K. The error of the density calculation at low temperatures was evaluated with allowance for the character of the deviations of the values in [6, 7] from the results of the generalization and at higher temperatures (Fig. la).

Sonic Velocity. Table 3 shows the experimental studies of sonic velocity in 1-pentanol. It can be seen that the most extensive measurements of sonic velocity at atmospheric pressure and on the saturation curve were obtained by Otpushchennikov and his co-authors [22, 24, 26-29]. There is one work [25] in which the speed of sound was measured in the low-temperature region at the frequency 23.6 MHz. However, it must be kept in mind that measurements at this frequency at low temperatures may be accompanied by dispersion of sound [2].

Preliminary analysis of the initial values showed that most of them agree with each other to within 0.1-0.2%. The exception is the data in [18, 19, 21, 23]. The results in [19] and [21] are low by 3 and 0.4-0.6%, respectively, in every instance compared to the other data, while the sonic velocities in [18] and [23] are overstated by 5 and 2-5%. We should point out the substantial deviations of the results in [21] from most of the data. This difference is more pronounced in view of the fact that nearly all of the other results

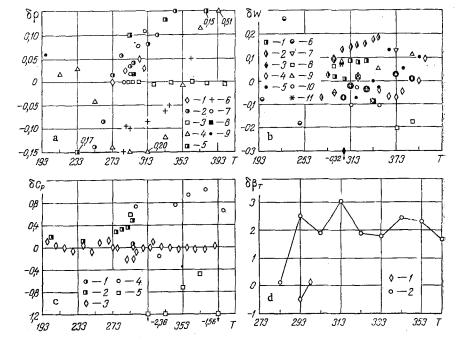


Fig. 1. Comparison of calculated values of density (a), sonic velocity (b), isobaric specific heat (c), and the coefficient of isothermal compression (d) with data of other authors:

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a) \delta \rho = (\rho \ [i] - \rho) \cdot 100/\rho, % (I - [3]; 2 - [4]; 3 - [5]; 4 - [6]; 5 - [7]; 6 - [9]; 7 - [13]; 8 - [14]; 9 - [8]); b) \delta W = (W \ [i] - W) \cdot 100/W, % (I - [11]; 2 - [13]; 3 - [20]; 4 - [22]; 5 - [24]; 6 - [25]; 7 - [26]; 8 - [27]; 9 - [28]; 10 - [29]; 11 - [30]); c) \delta C_p = (C_p \ [i] - C_p) \times 100/C_p, % (I - [4]; 2 - [31]; 3 - [32]; 4 - [33]; 5 - [34]); d) \delta \beta_T = (\beta_T \ [i] - \beta_T) \cdot 100/\beta_T, % (I - [38]; 2 - [39]);
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i is the number of the literature source. T, °K.

agree (to within 0.1-0.2%) for methanol and ethanol [1] and 1-propanol [2]. The deviations not only exceed the estimated error (about 0.05%) but also exceed the total error of the data being compared. The reasons for this discrepancy remain unclear.

In the final analysis made, we used the results from [11, 13, 22, 24-30].

The coefficients  $a_i$  for the speed of sound are shown in Table 1. Figure 1b shows deviations of the initial data from the results of the generalization. It can be seen from the figure that the deviations lie for the most part within the experimental error indicated in these studies, except for two empirical points in [25] at temperatures of 213.15 and 294.15 °K. The deviation here is 1%. The possible error of the recommended values of sonic velocity (see Table 2) can be evaluated as  $\pm 0.10\%$  at  $T \ge 273\%$ K. As concerns temperatures below 273°K the calculated values of sonic velocity have the same error here as the values in [25].

Isobaric Specific Heat. Four studies have investigated the specific heat  $C_P$  of 1-pentanol in the liquid phase. The study [31] measured  $C_P$  in the range from 204 to 298°K with an error of 0.5%. The most thorough investigation of specific heat on the saturation curve was made in [32], in which 54 empirical points were obtained at 300-389°K. The error of the data was evaluated as 0.1-0.2%. Also shown as a function of the temperature from the triple point (195.56°K) up to 390°K are smoothed values of  $C_P$ . The smoothing was done by means of a Chebyshev polynomial, the coefficients of which are not presented in the work. The value of  $C_P$  at the triple point was determined by the authors by graphical-analytical extrapolation of their data. In [33] specific heat was determined in the liquid phase in the temperature range 301-463°K and pressure range 0.098-0.81 MPa with an error of 0.9%. Specific heat was determined in [34] in the ranges T = 293-393°K and P = 0.1-60 MPa with an error of 1.5%. The values of  $C_P$  recommended in [4] for the melting and boiling points have errors of 2 and 5%.

We included all of the above-mentioned data in our analysis. The values of Cp on the saturation curve [32] were corrected for atmospheric pressure. The size of the correction did not exceed 0.01%.

TABLE 2. Calculated Values of the Density and Sonic Velocity of 1-Pentanol

Т	ρ	W		ρ	W
194,95 203,15 213,15 223,15 233,15 243,15 253,15 263,15 273,15 283,15 298,15	0,8870 0,8805 0,8728 0,8653 0,8578 0,8505 0,8433 0,8361 0,8290 0,8218 0,81452 0,81086	1667,7* 1631,4 1588,8 1547,8 1508,4 1470,2 1433,1 1397,0 1361,7 1327,0 1292,7 1275,8	303,15 313,15 323,15 333,15 343,15 353,15 363,15 373,15 383,15 393,15 403,15 411,13	0,80719 0,79974 0,79213 0,78434 0,77632 0,76804 0,75949 0,75061 0,74140 0,73188 0,72188	1258,9 1225,3 1191,8 1158,4 1125,0 1091,4 1057,7 1023,7 989,5 954,9 920,0 892,0

\*Extrapolation.

TABLE 3. Experimental Studies of Sonic Velocity in 1-Pentanol

Literature source	Number of points	Temperature range, °K	Error, %
[18] [19] [20] [11] [21] [13] [22] [23] [24] [25] [26] [27] [28] [29] [30]	1 2 1 6 Equation Equation 30 7 11 5 4 4 7 3 1	297,15 275,95; 301,65 303,15 293—343 273—353 293—583 293—413 303—403 198—294 293—373 293—373 293—393 293—423 313—353 303,15	

\*Error of approximation.

The coefficients  $a_i$  for  $C_P$  are shown in Table 1. Equation (1) describes the initial values with an error no greater than the error of the experiments (Fig. 1c). The most reliable results [32] are described with deviations not exceeding  $\pm 0.10\%$ , except for seven points for which the deviations lie within the range 0.1-0.2%. Since the recommended values of  $C_P$  [4] at the melting and boiling points have a large error, we employed graphical-analytical extrapolation of the data in [32, 33] to refine the values of specific heat  $C_P$  at the nodal points (Table 4).

The possible error of the recommended values of  $C_P$  can be evaluated as  $\pm 0.1\%$  in the temperature range 200-390°K and as  $\pm 0.2$  and  $\pm 0.5\%$  on the boundaries of this interval, including the nodal points.

It must be noted that the function  $C_P = f(T)$  for liquid 1-pentanol is of a peculiar nature. Results of calculations show that in the temperature range from the melting point to about 338°K an increase in temperature is accompanied by an increase in the derivative  $dC_P/dT$ . The derivative then reaches a maximum in the neighborhood of 338°K and decreases appreciably with a further increase in temperature. For example, the values of the derivative at T = 338.15°K and at the boiling point differ by a factor greater than two. This behavior of the temperature dependence of the specific heat of the alcohol is evidently due to intermolecular association [35], since it is known that the latter affects nearly all properties of liquids. This effect is even more pronounced for the higher alcohols [33, 36, 37].

<u>Calculation of the Thermodynamic Properties.</u> In calculating values of enthalpy, for the reference point we took the state of the liquid at the normal melting point  $(h_{mp}=0)$ . In accordance with this, the formula for the enthalpy of 1-pentanol at the temperature T, with allowance for Eq. (1), has the form

TABLE 4. Calculated Values of the Thermodynamic Properties of 1-Pentanol

\*Extrapolation.

$$h = h_{\rm mp} + \int_{T_{\rm mp}}^{T} C_p dT = 1000 \sum_{i=0}^{6} a_i (\tau^{i+1} - 0.19495^{i+1})/(i+1), \tag{2}$$

where  $a_i$  are coefficients of Eq. (1) for  $C_p$ .

Table 4 shows values of enthalpy of 1-pentanol calculated from Eq. (2). The same table gives results of calculation of  $C_V$ ,  $\beta_S$ , and  $\beta_T$  obtained with interpolation formulas for  $\rho^{-1}$ , W, and  $C_P$  and known thermodynamic relations. Figure 1d shows deviations of the calculated values of  $\beta_T$  from the experimental data [38, 39]. It can be seen from the figure that the values in [39] are 2% higher on the average. This is within the total error of the compared theoretical and empirical values. A comparison with theoretical values of  $C_{
m P}$  and  $C_{
m V}$  [40] at 293-393°K showed that the latter are too low relative to our values by an average of 10-20%.

## NOTATION

T, temperature according to MPShT-68°K;  $T_{mp}$ , melting point, °K;  $\rho$ , density,  $g/cm^3$ ; W, sonic velocity, m/sec;  $C_V$  and  $C_P$ , isochoric and isobaric specific heat, respectively, kJ/ (kg·K);  $\beta_{
m S}$  and  $\beta_{
m T}$ , coefficients of adiabatic and isothermal compression, 1/MPa;  $h_{
m mp}$  and h, enthalpy at the melting point and at the temperature T, kJ/kg.

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